TRANSITION TO HYDROGEN ECONOMY

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GENERAL PROPERTIES OF HYDROGEN

- Hydrogen is the 3rd abundant substance on earth.
- Not available as free H₂.
- Energy is required to free H₂ from its compounds.
- Combustion of Hydrogen produces H₂O. Nevertheless, its well to wheel LCA suggests only green H₂ is environmentally friendly.





Specific H₂ properties compared to other fossil fuels

| Property | Hydrogen | CNG | Gasoline | Diesel |
|---|---------------------|----------------------|------------------|------------------|
| Carbon content (mass%) | 0 | 75 ^e | 84 | 86 |
| Lower heating value (MJ/kg) | 119.7 | 45.8 | 44.8 | 42.5 |
| Density ^{a,b} (kg/m ³) | 0.089 | 0.72 | 730-780 | 830 |
| Volumetric energy content ^{a,b} (MJ/m ³) | 10.7 | 33.0 | 33×10^3 | 35×10^3 |
| Molecular weight | 2.016 | 16.043 e | ~ 110 | ~ 170 |
| Boiling point a (K) | 20 | 111 ^e | 298-488 | 453-633 |
| Auto-ignition temperature (K) | 858 | 813 ^e | ~623 | ~523 |
| Minimum ignition energy in air a,d (mJ) | 0.02 | 0.29 | 0.24 | 0.24 |
| Stoichiometric air/fuel mass ratio | 34.5 | 17.2 ^e | 14.7 | 14.5 |
| Stoichiometric volume fraction in air (%) | 29.53 | 9.48 | ~2 f | - |
| Quenching distance a,c,d (mm) | 0.64 | 2.1 ^e | ~2 | - |
| Laminar flame speed in air ^{a,c,d} (m/s) | 1.85 | 0.38 | 0.37-0.43 | 0.37-0.43 8 |
| Diffusion coefficient in air a,b (m2/s) | $8.5 	imes 10^{-6}$ | 1.9×10^{-6} | - | - |
| Flammability limits in air (vol%) | 4-76 | 5.3-15 | 1-7.6 | 0.6-5.5 |
| Adiabatic flame temperature a,c,d (K) | 2480 | 2214 | 2580 | ~2300 |

^a at 1 bar, ^b at 273 K, ^c at 298 K, ^d at stoichiometry, ^e methane, ^f vapor and ^g n-heptane.



H₂ PRODUCTION SMR

- 70 Mt/year is the world production of H_2 .
- 76% from CH_4 steam reforming.
- 23% from coal gasification.
- It consumes 6% of global CH_4 .
- And 2% of global coal.
- It releases 830 Mt/year of CO_2 .
- The price is $1/kg H_2$ in the middle east without CCUS.



H₂ PRODUCTION COST





H₂ PRODUCTION BY SMR

- Feedstock is CH₄ and steam.
- Steam works as oxidant and a source of H_2 .
- $30\sim40\%$ of CH₄ is used as fuel to elevate the temp. to 700~1100°C.
- Pressures as high as 25 bar are required.
- 6.6 m³ of water is required for 1t H_2 .

 $CH_{4 gas} + H_2O + Heat \rightarrow CO_{gas} + 3H_{2 gas}$

• Syngas is treated in a water gas shift process.

 $CO_{gas} + H_2O_{gas} \rightarrow CO_{2\,gas} + H_{2\,gas} + Heat$

• CCUS could reduce CO₂ by 90% to upgrade the renewability of SMR.







- The cost to produce 1.1 t H_2 is \$590.
- Electricity \$217 and \$373 for power gas.





- The cost to produce 1.1t H_2 is \$1,091.
- Electricity \$217, CCUS \$377 and \$497 for power gas.



H₂ Production by CH₄ Pyrolysis



- It requires more methane gas but less energy.
- No CO₂.
- Solid carbon is a by-product for reuse in tyre industry.
- The cost to produce $1.1tH_2$ is \$944.



The cost is subdivided to \$198 electricity and \$746 power gas

CARBON CAPTURE For USAGE AND STORAGE

- To upgrade the level of renewability of H₂.
- The cost for 60% CO₂ removal from syngas is \$ 53/t CO₂.
- 90% CO₂ removal increases the cost to \$80/t CO₂.





H₂ Production by Water Electrolysis

- Provides only 0.1% of dedicated H₂.
- Very pure H₂, mainly used in electronics industry and polysilicon.
 2H₂O + electricity → 2H₂ + O₂
- 1kg H_2 is produced from 9kg H_2 O.
- Low carbon emission.
- Could be upgraded to Net Zero Carbon by green electricity.





H₂ PRODUCTION BY WATER Electrolysis

- 3,600 TWh electricity is needed to shift to H_2 production by water electrolysis.
- This is more than the annual EU electricity generation.
- 617 Mm³ fresh water is needed.
- This is twice the H_2O needed for SMR and 1.3% of H_2O consumption in the energy sector.







- 3~4 kWh is needed to desalinise sea water by reverse osmosis.
- This will add a cost of $0.7 \sim 2.5/m^3$ of water.
- The cost of H_2 production increases by \$0.01~0.02/kg H_2 .



