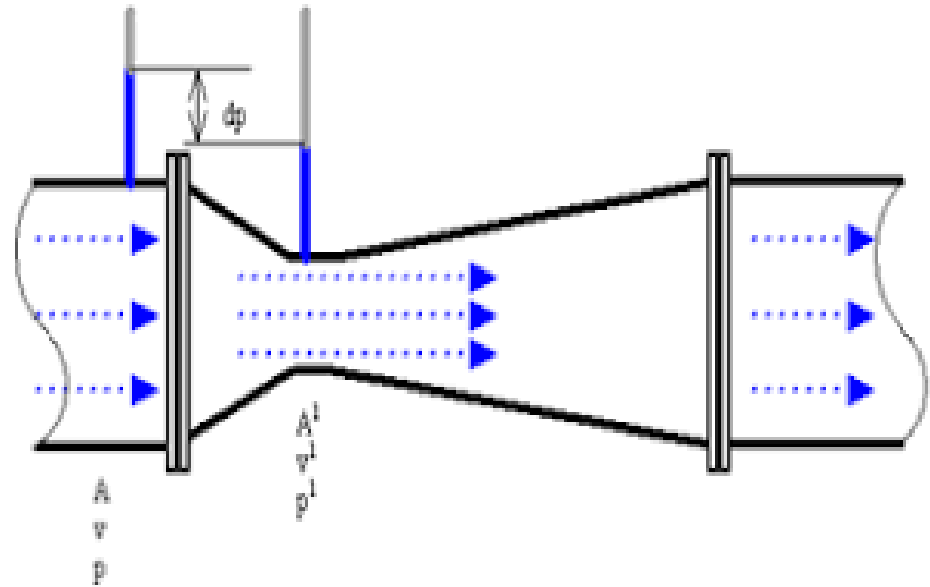


APPLICATION ON BERNOULLI EQUATION

VENTURI METER

VENTURI METER

A venturi meter is a device used to measure the fluid flow through pipes. This flow measurement device is based on the principle of Bernoulli's equation. Inside the pipe, pressure difference is created by reducing the cross-sectional area of the flow passage. This difference in pressure (heads) is measured with the help of manometer and helps in determining rate of fluid flow or other discharge from the pipe line. As the main inlet area is more as compared to throat, velocity of fluid at throat increases therefore pressure decreases. By this, a pressure difference is created between the inlet and the throat of the venturi meter. Hence, by reducing the cross-sectional area of the flow passage, a pressure difference is created and we measure that difference in pressure by using Bernoulli equation and discharge formula (Continuity equation).

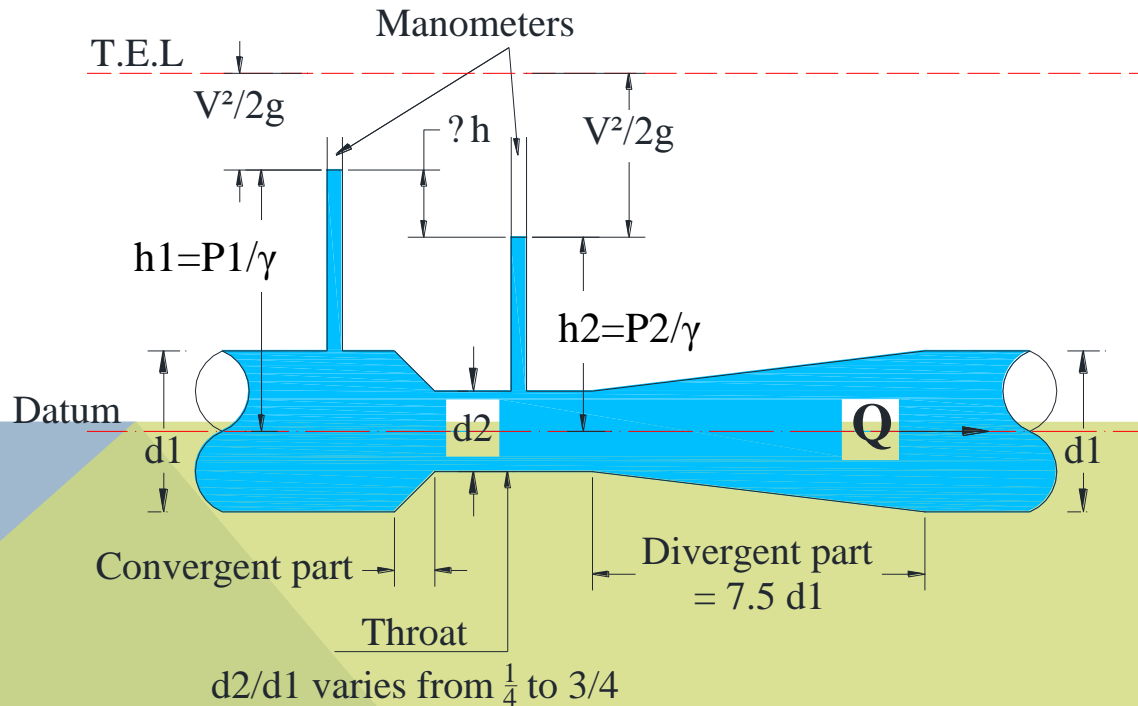


Applying Bernoulli equation, for theoretical condition

$$\frac{P_1}{\gamma_1} + \frac{V_{1theo}^2}{2g} + Z_1 = \frac{P_2}{\gamma_2} + \frac{V_{2theo}^2}{2g} + Z_2$$

For horizontal Venturi meter

$$h_1 + \frac{V_{1theo}^2}{2g} = h_2 + \frac{V_{2theo}^2}{2g} \quad \Rightarrow \quad h_1 - h_2 = \frac{V_{2theo}^2}{2g} - \frac{V_{1theo}^2}{2g} \quad \dots\dots 1$$



Applying Continuity equation between section 1 & 2

$$Q_{theo1} = Q_{theo2}$$

$$Q_{theo} = V_1 A_1 = V_2 A_2 \Rightarrow V_1 = V_2 \frac{A_2}{A_1}$$

Substituting equation 2 in 1

$$h_1 - h_2 = \frac{V_{2theo}^2}{2g} - \frac{\left(\frac{A_2}{A_1}\right)^2 V_{2theo}^2}{2g}$$

$$h_1 - h_2 = \frac{V_2^2 - \left(\frac{A_2}{A_1}\right)^2 V_2^2}{2g} \Rightarrow h_1 - h_2 = \frac{V_2^2 [1 - \left(\frac{A_2}{A_1}\right)^2]}{2g}$$

$$V_{2theo}^2 = \frac{2g(h_1 - h_2)}{[1 - \left(\frac{A_2}{A_1}\right)^2]} \Rightarrow V_{2theo} = \sqrt{\frac{2g(h_1 - h_2)}{[1 - \left(\frac{A_2}{A_1}\right)^2]}}$$

$$Q_{theo} = A_2 V_2 \ ; \ Q_{act} = C_d Q_{theo} \ ; \ C_d = (0.9 - 0.98); \ C_d = C_v \ ; \ C_c = 1$$

$$\frac{D_2}{D_1} = \frac{1}{4} \text{ to } \frac{3}{4} \ ; \text{ usually } \frac{D_2}{D_1} = \frac{1}{2}$$

C_d = discharge coefficient

C_v = velocity coefficient

C_c = contraction coefficient

A_1 = cross section area of the pipe

A_2 = cross section area of the throat

Example : Determine the actual discharge through the Venturi meter if diameter of throat $D_2 = 5$ cm, and the pipe diameter $D_1 = 10$ cm, having a difference in pressure 50 kpa and $C_d = 0.98$

Solution:- different in pressure (Δh) = $h_1 - h_2$

$$\Delta p = 50 \text{ Kpa}, \quad \Delta h = \frac{\Delta p}{\gamma} = \frac{50 * 1000}{9806} = 5.0989 \text{ m}$$

$$A_1 = \frac{\pi D_1^2}{4} = \frac{\pi}{4} (0.1)^2 = 0.007854 \text{ m}^2 ; \quad A_2 = \frac{\pi D_2^2}{4} = \frac{\pi}{4} (0.05)^2 = 0.001963 \text{ m}^2$$

$$Q_{theo} = V_2 A_2 = A_2 \sqrt{\frac{2g(h_1 - h_2)}{[1 - (\frac{A_2}{A_1})^2]}} = 0.001963 \sqrt{\frac{2g(5.0989)}{[1 - (\frac{0.001963}{0.007854})^2]}}$$
$$= 0.0203 \text{ m}^3/\text{sec}$$

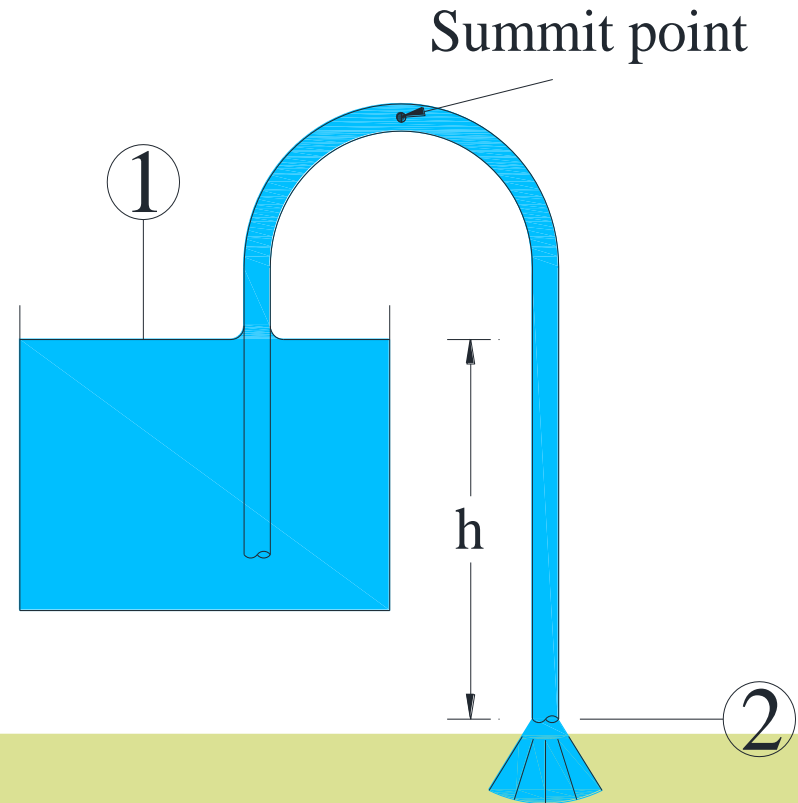
$$Q_{act} = C_d Q_{theo} = 0.98 * 0.0203 = \mathbf{0.0199 \text{ m}^3/\text{sec}}$$

APPLICATION ON BERNOULLI EQUATION

SIPHON

SIPHON

A long bend pipe, used to carry water from a reservoir at a higher level to another reservoir at a lower level when two reservoirs are separated by a hill, is called as siphon. The highest point of siphon is called as summit. The highest point of siphon lies above the free water surface in the reservoir at higher level. Therefore, pressure at this point is below atmospheric. The negative or vacuum pressure is created in the siphon, so that liquid gets pushed into it. Siphon works on Bernoulli's principle and it is used when the water have to take out from reservoir to another separated by a hill. Siphon is also used to drain out water from a channel without any outlet. The siphon it is used for determine velocity and losses through it.



Applying Bernoulli equation between 1 & 2 without losses

$$\frac{P_1}{\gamma} + \frac{V_{1theo}^2}{2g} + Z_1 = \frac{P_2}{\gamma} + \frac{V_{2theo}^2}{2g} + Z_2$$

$$0 + 0 + h = 0 + \frac{V_2^2}{2g} + 0$$

$$V_2 = \sqrt{2g Z_1} \Rightarrow V_2 = \sqrt{2gh}$$

If losses exist, the equation will be:

$$\frac{P_1}{\gamma} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\gamma} + \frac{V_2^2}{2g} + Z_2 + losses$$

$$0 + 0 + h = 0 + \frac{V_2^2}{2g} + 0 + h_f$$

$$Losses = h_f = f \frac{L}{D} \frac{V_2^2}{2g}$$

$$h - h_f = \frac{V_2^2}{2g} \Rightarrow V_2 = \sqrt{2g (h - h_f)}$$

Example: the siphon of fig. is filled with water and is discharging at 150 L/sec. Find the losses coefficient (k) from point 1 to point 3 in terms of velocity head $k \frac{V^2}{2g}$. Find the pressure at point 2.

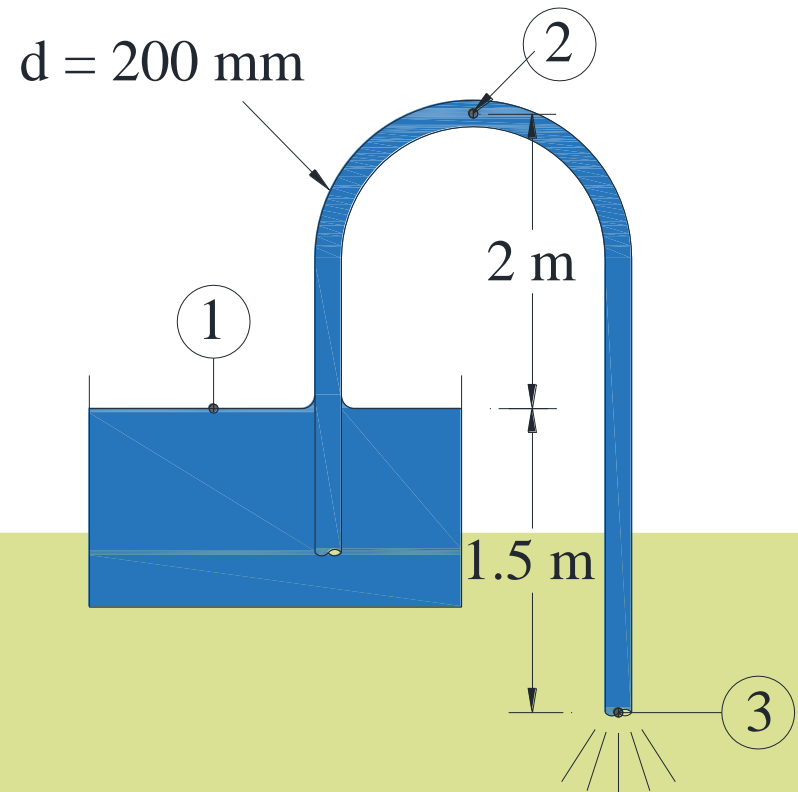
Solution:-
$$\frac{P_1}{\gamma} + \frac{V_1^2}{2g} + Z_1 = \frac{P_3}{\gamma} + \frac{V_3^2}{2g} + Z_3 + \text{Losses}_{1-3}$$

$$0 + 0 + 1.5 = 0 + \frac{V_3^2}{2g} + 0 + k \frac{V_3^2}{2g}$$

$$V_3 = \frac{Q}{A} = \frac{\frac{150}{1000}}{\frac{\pi}{4} \left(\frac{200}{1000}\right)^2} = 4.77 \text{ m/sec}$$

$$1.5 = 1.16 + k \frac{V_3^2}{2g} \Rightarrow k \frac{V_3^2}{2g} = 0.34 \text{ m}$$

$$k = 0.29$$



The pressure head at 2

$$\frac{P_1}{\gamma} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\gamma} + \frac{V_2^2}{2g} + Z_2 + \text{Losses}_{1-2}$$

$$0 + 0 + 0 = \frac{P_2}{\gamma} + \frac{(4.77)^2}{2g} + 2 + \left(\frac{2}{(2 + 2 + 1.5)} \right) 0.29 \frac{(4.77)^2}{2g}$$

$$\frac{P_2}{\gamma_2} = -3.2825 \text{ m}$$

$$P_2 = -32188.14836 \text{ N/m}^2$$

* The negative sign mean the pressure is suction for continuity the flow.