



## Module ( Course Syllabus ) Catalogue 2023-2024

College/ Institute	Erbil Technical Engineering College	
Department	Mechanical and Energy Engineering Techniques	
Module Name	Two Phase Flow	
Module Code	TPF104	
Degree	Technical Diploma <input type="checkbox"/>	Bachler <input type="checkbox"/>
	High Diploma <input type="checkbox"/>	Master <input type="checkbox"/> D <input checked="" type="checkbox"/>
Semester	Fall	
Qualification	Thermal Powers – Heat and Mass Transfer	
Scientific Title	Assistance Professor	
ECTS (Credits)	05	
Module type	Prerequisite <input type="checkbox"/>	Core <input checked="" type="checkbox"/> Assist. <input type="checkbox"/>
Weekly hours		
Weekly hours (Theory)	( 03 )hr Class	( 06 )Total hrs Workload
Weekly hours (Practical)	( )hr Class	( )Total hrs Workload
Number of Weeks	15	
Lecturer (Theory)	Asst. Prof. Dr. Mohammed Jawdat Barzanjy	
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Lecturer (Practical)		
E-Mail & Mobile NO.		
Websites		

# Course Book

<b>Course Description</b>	<p>Two phase flow with or without phase change is commonly encountered in a variety of engineering processes. The power generation, nuclear reactor technology, food production, chemical process, aerospace and automotive industries are all driving forces in this complex field. Due to its universality in applications, a thorough understanding of two phase flow is of utmost important. Present course is driven by this requirement.</p> <p>Two Phase Flow, is a well established topic in Mechanical and chemical engineering, taught to the post – graduate students as follows:</p> <ol style="list-style-type: none"><li>1. A theoretical weekly program of three hours.</li><li>2. A workload weekly program of six hours.</li></ol>
<b>Course objectives</b>	<ol style="list-style-type: none"><li>1. Acquire specialized knowledge in modelling the engineering problems and solve by new methods with good accuracy.</li><li>2. Use the update advanced numerical methods and compare the results with the engineering analysis methods results</li><li>3. Opportunity of deep analysis of advanced engineering and numerical methods.</li></ol>
<b>Student's obligation</b>	<p>For the student to achieve a level of excellence in the subject, the following items should be given utmost consideration:</p> <ol style="list-style-type: none"><li>a. Class attendance on regular basis for the purpose of learning.</li><li>b. Active participation in class discussions.</li><li>c. Reviewing the lecture notes and topics on weekly basis, noting the ambiguous points, if any, and requesting clarification during instructor office hours..</li><li>d. Giving adequate and sufficient priority to preparing for weekly, monthly and final tests.</li></ol>
<b>Required Learning Materials</b>	<p>Due to very equations and rules driving, the essence of teaching program is presented on white board. Sometimes, some explanations of details are prepared on MS power point. There are also assignments and seasonal projects appointed to individual students or groups that help the evaluation process and also support team work effort.</p>

<b>Evaluation</b>	<b>Task</b>	<b>Weight (Marks)</b>	<b>Due Week</b>	<b>Relevant Learning Outcome</b>	
	Paper Review				
	Assignments	Homework			
		Class Activity	05		
		Report	05		
		Seminar	10		
		Essay			
		Project			
	Quiz	10			
	Lab.				
	Midterm Exam	20			
	Final Exam	50			
	Total	100			
<b>Specific learning outcome:</b>	<p>Upon completion of the subject, students will be able to:</p> <p>a. Obtain fundamental knowledge in the area of modes of Two Phase Flow.</p> <p>b. Apply their knowledge, skills and hand-on experience to the analysis of flow in change phase.</p> <p>c. Extend their knowledge of mechanical engineering to different situations of engineering context and professional practice in Transforming Phenomenon.</p> <p>d. Recognize the need for and an ability to engage in life-long learning.</p>				
<b>Course References:</b>	<ol style="list-style-type: none"> <li>Ghiaasiaan, S. M., Two-Phase flow, Boiling, and Condensation, Cambridge University Press.</li> <li>Brennen, C.E., Fundamentals of Multiphase Flow, Cambridge University Press.</li> <li>Collier, J. G. and Thome, J. R., Convective Boiling and Condensation, 3rd ed., Oxford University Press.</li> <li>Wallis, G.B., One Dimensional Two Phase Flow, McGraw Hill Higher Education.</li> </ol>				

Course topics (Theory)	Week	Learning Outcome
What is Two Phase Flow .. ?	1	
Flow regimes and notation	2	
Flow patterns and flow regime maps	3	
Momentum equation for two-phase flow	4	
Flow in bubble columns	5	
Mid – Semester Examination	6	
Pressure drop Bubble rise velocity	7	
Slug flow in vertical tubes	8	
Seminar	9	
The homogeneous model for two-phase flow Momentum equation for the homogeneous flow model	10	
Friction factors for the homogeneous model	11	
Two-phase multiplier	12	
Separated flow models - I	13	
Separated flow models – II	14	
Final Semester Examinations	15	

## Questions Example Design

*Note: Attempt all the questions.*

**Q1.** Choose the correct answer for each of the following:

**20 Marks**

1. Mass transfer takes place ...	(a) in a multi phase (b) in a double phase (c) only in a single phase
2. The fluid moves under the influence of an external force is .....	(a) Forced convection (b) Natural convection (c) Free convection
3. If there is any variation in density within the fluid phase, the ..... currents develop	(a) Forced convection (b) Natural convection (c) Diffusion
4. Momentum transfer as given by	(a) $J_A = -D_{AB} \frac{dC_A}{dz}$ (b) $q = -k \frac{dT}{dz}$ (c) $\tau = -\mu \frac{dv}{dz}$
5. Reynolds postulated that the mechanisms for transfer of ( Momentum, Energy and Mass ) are identical. Accordingly,	(a) $f / 2$ (b) $f / 3$ (c) $f / 4$
6. Based on data collected in both ( Laminar and Turbulent ) flow regimes, they found that:	(a) $j_D = j_H = \frac{f}{4}$ (b) $j_D = j_H = \frac{f}{3}$ (c) $j_D = j_H = \frac{f}{2}$
7. $Sh = 0.664 Re_L^{1/2} Sc^{1/3}$	(a) (Laminar) $Re_L < 2 - 5 \cdot 10^5$ (b) (Laminar) $Re_L < 2 - 4 \cdot 10^5$ (c) (Laminar) $Re_L < 2 - 3 \cdot 10^5$

8. For very low ( Re ), the ( Sh )	(a) $Sh = 2 + C Re^m Sc^{1/2}$ (b) $Sh = 2 + C Re^m Sc^{1/3}$ (c) $Sh = 3 + C Re^m Sc^{1/3}$
9. Mass transfer from the inner wall of a tube to a moving fluid is	(a) $Sh = 0.023 Re^{0.83} Sc^{0.44}$ (b) $Sh = 0.023 Re^{0.83} Sc^{0.55}$ (c) $Sh = 0.033 Re^{0.83} Sc^{0.44}$
10. Henry's law is	(a) $P_{Ai} = C_{Ai} / H$ (b) $P_{Ai} = H / C_{Ai}$ (c) $P_{Ai} = H C_{Ai}$
11. In the study of convective heat transfer, the heat flux is connected to heat transfer coefficient as:	(a) $Q/A = q = h(t_s - t_m)$ (b) $Q/A = q = h(t_m - t_s)$ (c) $Q/A = q = h.l(t_s - t_m)$
12. The analogous situation in mass transfer is handled by an equation of the form:	(a) $N_A = k_c (C_A - C_{As})$ (b) $N_A = k_c (C_{As} - C_A)$ (c) $N_A = k_c l (C_{As} - C_A)$
13. Prandtl Number = Pr = .....	(a) thermal diffusivity / mass diffusivity (b) momentum diffusivity / mass diffusivity (c) momentum diffusivity / thermal diffusivity
14. Schmidt Number = Sc = .....	(a) thermal diffusivity / mass diffusivity (b) momentum diffusivity / mass diffusivity (c) momentum diffusivity / thermal diffusivity
15. Lewis Number = Le = .....	(a) thermal diffusivity / mass diffusivity (b) momentum diffusivity / mass diffusivity (c) momentum diffusivity / thermal

		diffusivity	
	16. the equation for energy transport by Convection and molecular Diffusion becomes .....	(a) $q = h\Delta T + \sum_i N_i \bar{H}_i$ (b) $q = h\Delta T + \sum_i N_i / \bar{H}_i$ (c) $q = h / \Delta T + \sum_i N_i \bar{H}_i$	
	17. The molar flux ( $N_A$ ) is calculated by diffusion through stagnant gas model as .....	(a) $N_A = \frac{-C}{1-y_A} \frac{dy_A}{dZ}$ (b) $N_A = \frac{-CD_{AB}}{1-y_A} \frac{dy_A}{dZ}$ (c) $N_A = \frac{-D_{AB}}{1-y_A} \frac{dy_A}{dZ}$	
	18. To find humidity, we can write equation for the mass and energy fluxes as .....	(a) $N_A = k_c (C_{Ai} - C_A) = k_y (y_{Ai} + y_A)$ (b) $N_A = k_c (C_{Ai} + C_A) = k_y (y_{Ai} - y_A)$ (c) $N_A = k_c (C_{Ai} - C_A) = k_y (y_{Ai} - y_A)$	
	19. In the air - film surroundings, the wet - bulb, the mass and energy fluxes are coupled as .....	(a) $N_A \lambda = q$ (b) $N_A / \lambda = -q$ (c) $N_A \lambda = -q$	
	20. in the wet – bulb Thermometer .....	(a) $T_i = T - \frac{\lambda}{C_p} (y_{Ai} - y_A)$ (b) $T_i = T \frac{\lambda}{C_p} (y_{Ai} - y_A)$ (c) $T_i = T - \frac{2\lambda}{C_p} (y_{Ai} - y_A)$	
<b>Q2.</b>	A solid disc of benzoic acid ( 3 cm ) in diameter is spin at ( 20 rpm ) and ( 25°C ). Calculate the rate of dissolution in a large volume of water. Diffusivity of benzoic acid in water is ( $1.0 * 10^{-5} \text{ cm}^2 / \text{s}$ ), and solubility is ( $0.003 \text{ g} / \text{cm}^3$ ). The following mass transfer correlation is applicable:  $\text{Sh} = 0.62 \text{ Re}^{1/2} \text{ Sc}^{1/3}$		<b>35 Marks</b>

Where:  $Re = \frac{D^2 \omega \rho}{\mu}$ ,  $\omega$  - An angular speed in ( rad / s ).

**Q3.** A very thin polymeric coating of thickness ( 0.1 mm ) uniformly coats a rectangular surface. The rectangular surface has a length of ( 20 cm ) and a width of ( 10 cm ). The coating contains a solvent that must be evaporated away from the coating in order to cure the coating. Initially, there is ( 0.001 mole ) of solvent per ( cm<sup>3</sup> ) of coating loaded in the coating. A heated plate just beneath the surface maintains the coating at a uniform temperature of ( 40 °C ), and the vapor pressure exerted by the solvent is ( 0.05 atm ) at ( 40 °C ). Air gently flows parallel to the surface at a velocity of ( 5.0 cm/s ). The surrounding air at ( 1.0 atm ) total system pressure and ( 20 °C ) represents an “infinite sink” for mass transfer. You may neglect any molecular diffusion of the solvent through the very thin polymeric film and focus only on the convection aspects of the problem.

**45 Marks**

( a ) What is the average mass transfer coefficient (  $k_c$  ) ?

( b ) How long will it take for the solvent to completely evaporate from the coating ?

Given

The physical properties at 303 K are:

Kinematic viscosity  $\nu = 0.158 \text{ cm}^2 / \text{s}$

Density  $\rho = 1.17 \times 10^{-3} \text{ g} / \text{cm}^3$

The diffusion coefficient of species in air at ( 30 °C ),  $D_{AB} = 1.025 \text{ cm}^2 / \text{s}$

Correlation

$$Sh_L = 0.664 Re_L^{0.5} Sc^{0.33}$$

$$Sh_L = 0.0365 Re_L^{0.8} Sc^{0.33}$$

Conditions

( Laminar )  $Re_L < 2 \times 10^5$

( Turbulent )  $Re_L > 2 \times 10^5$

**Extra notes:**

Due to a number of unforeseen reasons that may lead to shifting of the academic semester program, it may be subjected to modifications. Also extra curriculum hours may be needed to cover all the topics. The students shall be notified of the changes if and when they may occur.

**External Evaluator**